

Suppression of 3D flow instabilities in tightly packed tube bundles

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Outline

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2. Goals

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4. Numerical method

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5. Results

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6. Conclusions

Introduction

Transition from 2D to 3D flow past an obstacle

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- Well understood for flow past a single tube.

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Transition from 2D to 3D flow past an obstacle

- Well understood for flow past a single tube.
- **Not** well understood for flow past a tightly packed tube bundle, e.g. spacing $P/D = 1.5$.

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Introduction (cont.)

Transition from 2D to 3D flow past a single tube

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Transition from 2D to 3D flow past a single tube

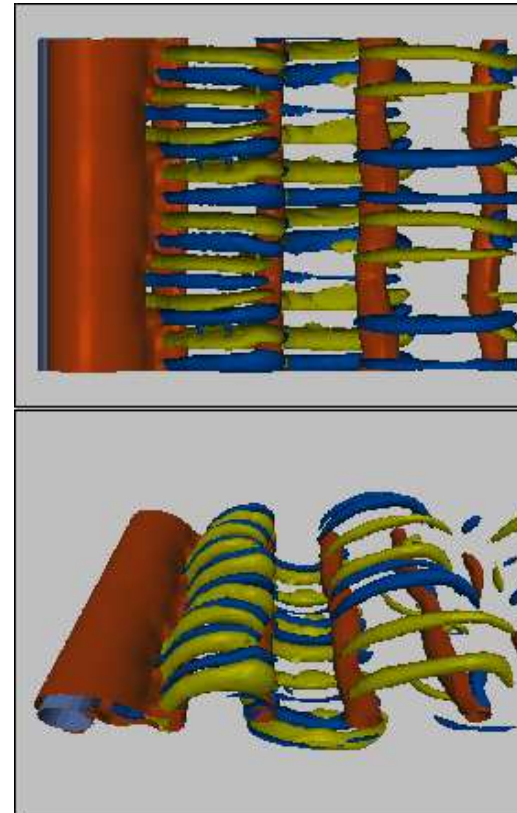
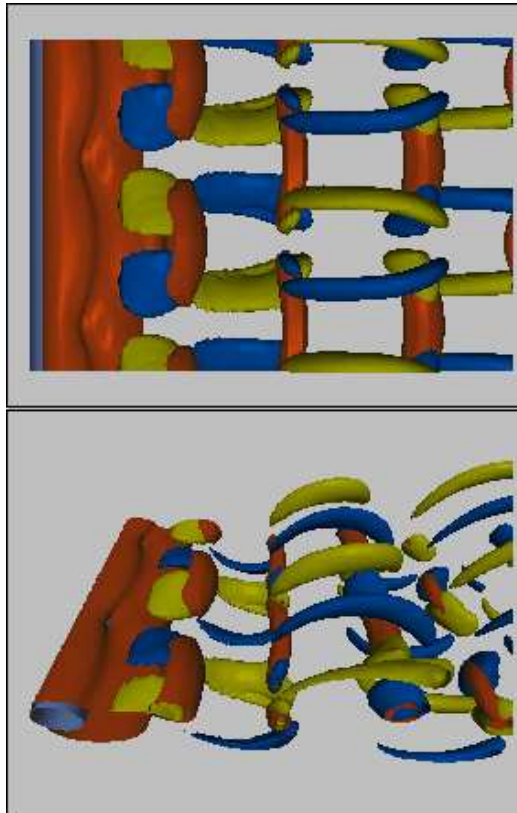
- Wake becomes 3D at $Re \approx 180$ via formation of streamwise vortices with a spacing of about three cylinder diameters (mode A instability)

Introduction (cont.)

Transition from 2D to 3D flow past a single tube

- Wake becomes 3D at $Re \approx 180$ via formation of streamwise vortices with a spacing of about three cylinder diameters (**mode A instability**)
- At $Re \approx 230$ a second vortex mode appears (**mode B instability**), via the formation of irregular streamwise vortices with a spacing of one cylinder diameter (Williamson 1989)

Introduction (cont.)



Mode A instability at $Re = 210$ Mode B instability at $Re = 250$
(Thompson, Hourigan & Sheridan 1995)

Introduction (cont.)

- As Reynolds number increases further, the wake becomes increasingly complicated until it is completely **turbulent**.



Introduction (cont.)

What about tightly packed tube bundles?



Industrial heat exchanger

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Introduction (cont.)

Transition from 2D to 3D flow past a tube bundle

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Transition from 2D to 3D flow past a tube bundle

- Experiments appear to indicate that the flow and cylinder response remain roughly two-dimensional for $Re \gg 180$ (Weaver 2001).

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Transition from 2D to 3D flow past a tube bundle

- Experiments appear to indicate that the flow and cylinder response remain roughly two-dimensional for $Re \gg 180$ (Weaver 2001).
- Price et al (1995) find that Strouhal frequency and rms drag do not change with Reynolds number for $Re > 150$.

Introduction (cont.)

- Blevins (1985) demonstrated that acoustic forcing of an isolated cylinder at its Strouhal frequency is able to produce nearly perfect spanwise correlation of pressure for $20\,000 \leq Re \leq 40\,000$.

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He conjectured that similar effects might be observed in tube bundles.

- This confirmed earlier work by Toebees (1969) showing cylinder vibration of $A/D \geq 0.125$ is required to enforce spanwise correlation.

Goals

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 - Is tight packing sufficient?
 - Is resonant tube motion effective in tube bundles?
 - Is tube motion amplitude large enough in tube bundles?
 - Does tube response remain 2D even if the flow is 3D?

Goals (cont.)

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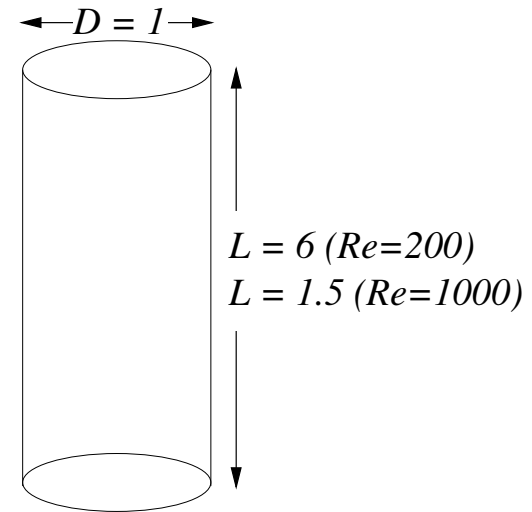
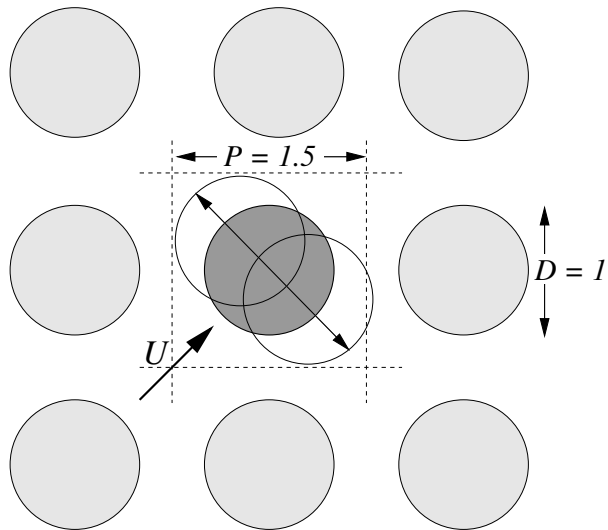
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Goals (cont.)

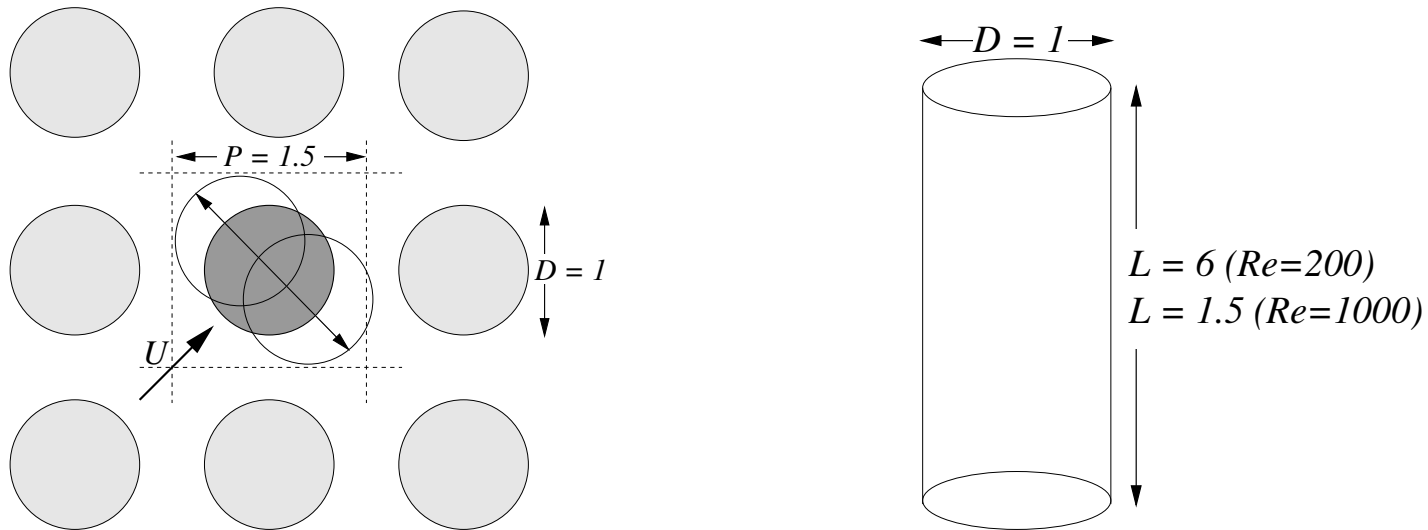
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 - What are the differences between 2D and 3D flows?
 - What are the differences in tube response?

We consider flows at $Re = 200$ and $Re = 1000$ in rotated square tube bundles with $P/D = 1.5$.

Problem formulation

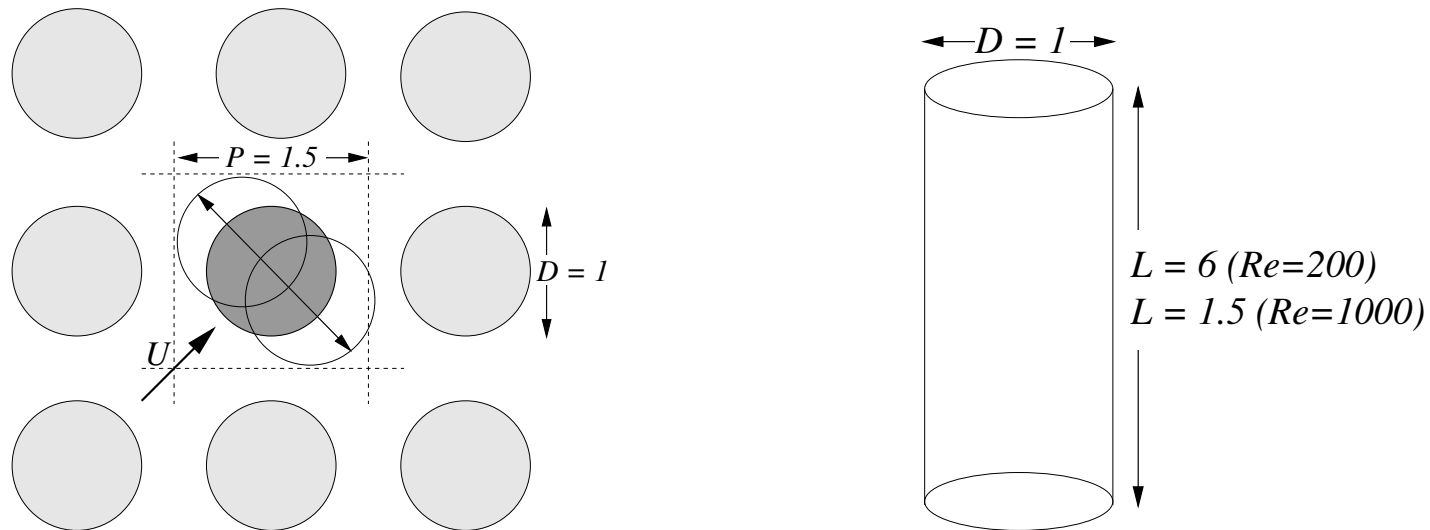


Problem formulation



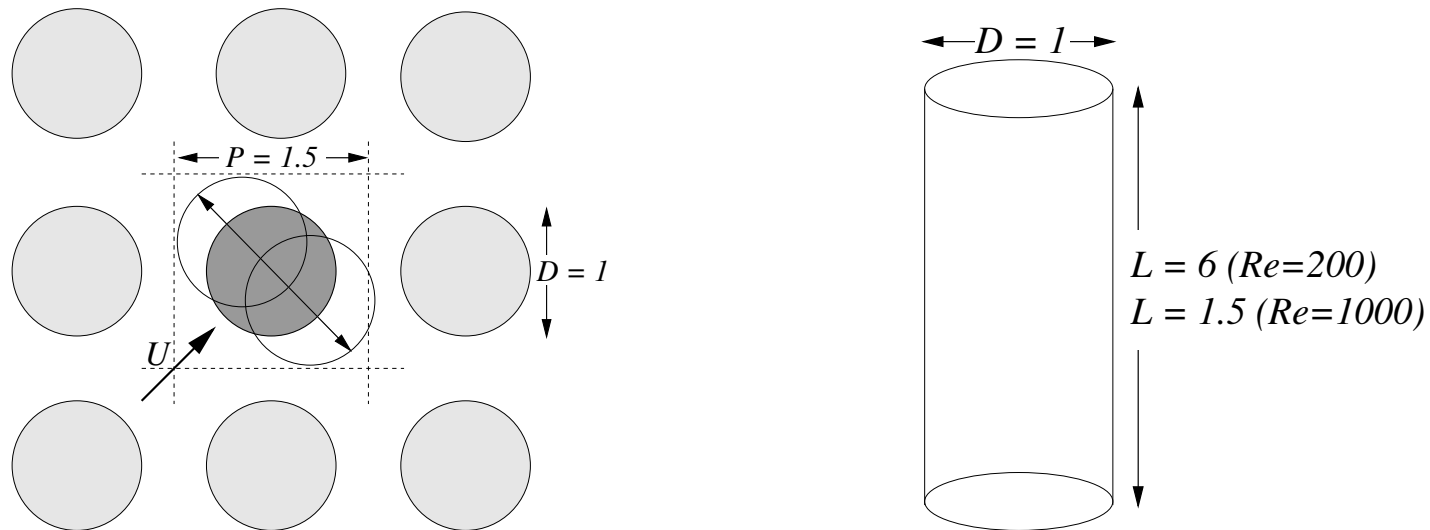
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Problem formulation



- Periodic boundary conditions.
- One tube in the periodic domain.

Problem formulation



- Periodic boundary conditions.
- One tube in the periodic domain.
- **All** tubes move in phase (extreme case).

Problem formulation (cont).

No-slip boundary conditions at tube surface

- Modelled by Brinkman penalization of Navier–Stokes equations.

$$\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} + \mathbf{U}) \cdot \nabla \mathbf{u} + \nabla P = \nu \Delta \mathbf{u}$$

$$\nabla \cdot \mathbf{u} = 0$$

Problem formulation (cont).

No-slip boundary conditions at tube surface

- Modelled by Brinkman penalization of Navier–Stokes equations.

$$\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} + \mathbf{U}) \cdot \nabla \mathbf{u} + \nabla P = \nu \Delta \mathbf{u} - \frac{1}{\eta} \chi(\mathbf{x}, t) (\mathbf{u} + \mathbf{U} - \mathbf{U}_o)$$
$$\nabla \cdot \mathbf{u} = 0$$

Problem formulation (cont.)

where the solid is defined by

$$\chi(\mathbf{x}, t) = \begin{cases} 1 & \text{if } \mathbf{x} \in \text{solid,} \\ 0 & \text{otherwise.} \end{cases}$$

- The upper bound on the global error of this penalization was shown to be (Angot et al. 1999) $O(\eta^{1/4})$.
- We observe an error of $O(\eta)$.

Problem formulation (cont.)

Cylinder response

- modelled as a damped harmonic oscillator

$$m\ddot{\mathbf{x}}_o(t) + b\dot{\mathbf{x}}_o(t) + k\mathbf{x}_o = \mathbf{F}(t),$$

Problem formulation (cont.)

Cylinder response

- modelled as a damped harmonic oscillator

$$m\ddot{\mathbf{x}}_o(t) + b\dot{\mathbf{x}}_o(t) + k\mathbf{x}_o = \mathbf{F}(t),$$

where the force $\mathbf{F}(t)$ is calculated from the penalization

$$\mathbf{F}(t) = \frac{1}{\eta} \int \chi(\mathbf{x}, t) (\mathbf{u} + \mathbf{U} - \mathbf{U}_o) d\mathbf{x}.$$

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Numerical method

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1. **Pseudo-spectral method** for calculating derivatives and nonlinear terms on the periodic spatial domain.
2. **Krylov time scheme** for adaptive, stiffly stable integration in time.

Results

Cases:

Re	resolution	L	m_*	b_*	k_*	f
200	$128^2 \times 64$	6.0	5	0	249	0.98
1 000	$288^2 \times 96$	1.5	5	0	130	1.00

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- Moving tubes are **tuned** to match the Strouhal frequency.

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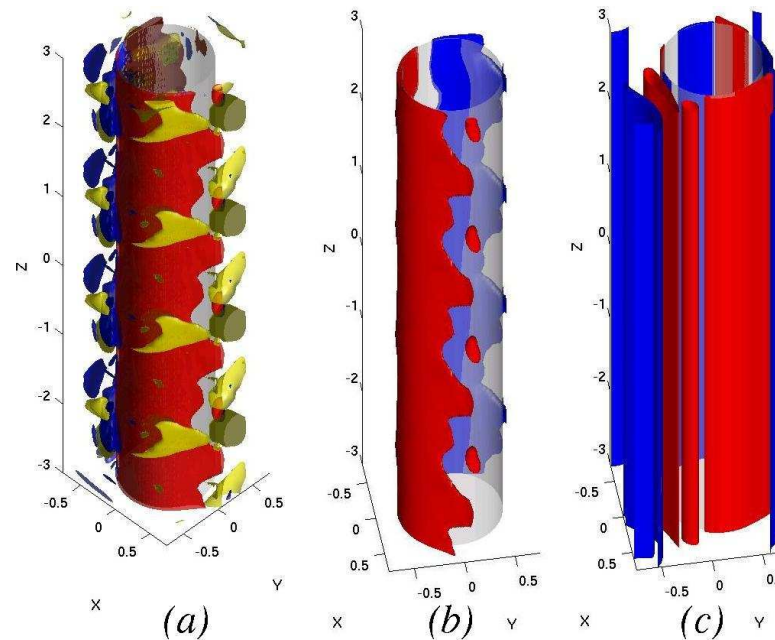
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- **Fixed and moving** tube simulations are done for each case.
- Moving tubes are **tuned** to match the Strouhal frequency.
- **2D** simulations are also done for each case.

$Re = 200$ results

Vorticity at $t = 15$

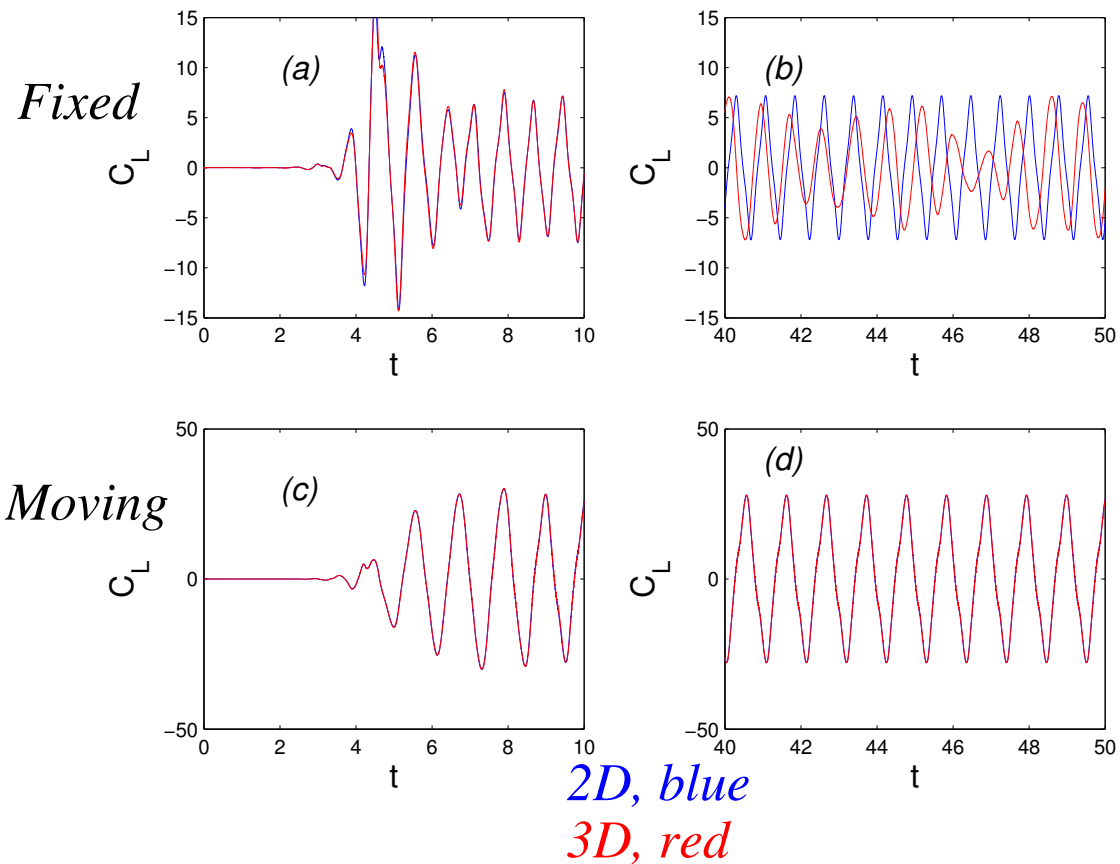


(a) Fixed cylinder, 3 components. (b) Fixed cylinder, spanwise vorticity.

(c) Moving cylinder, spanwise vorticity.

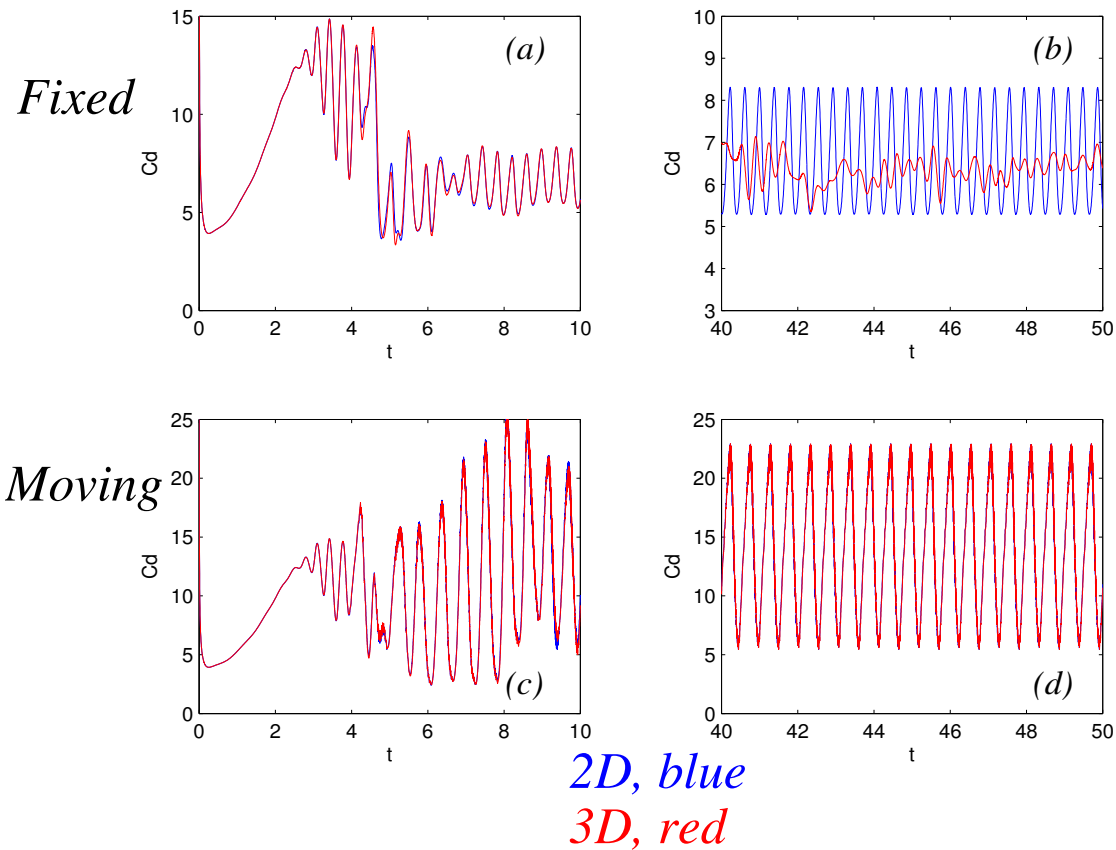
$Re = 200$ results (cont.)

Lift



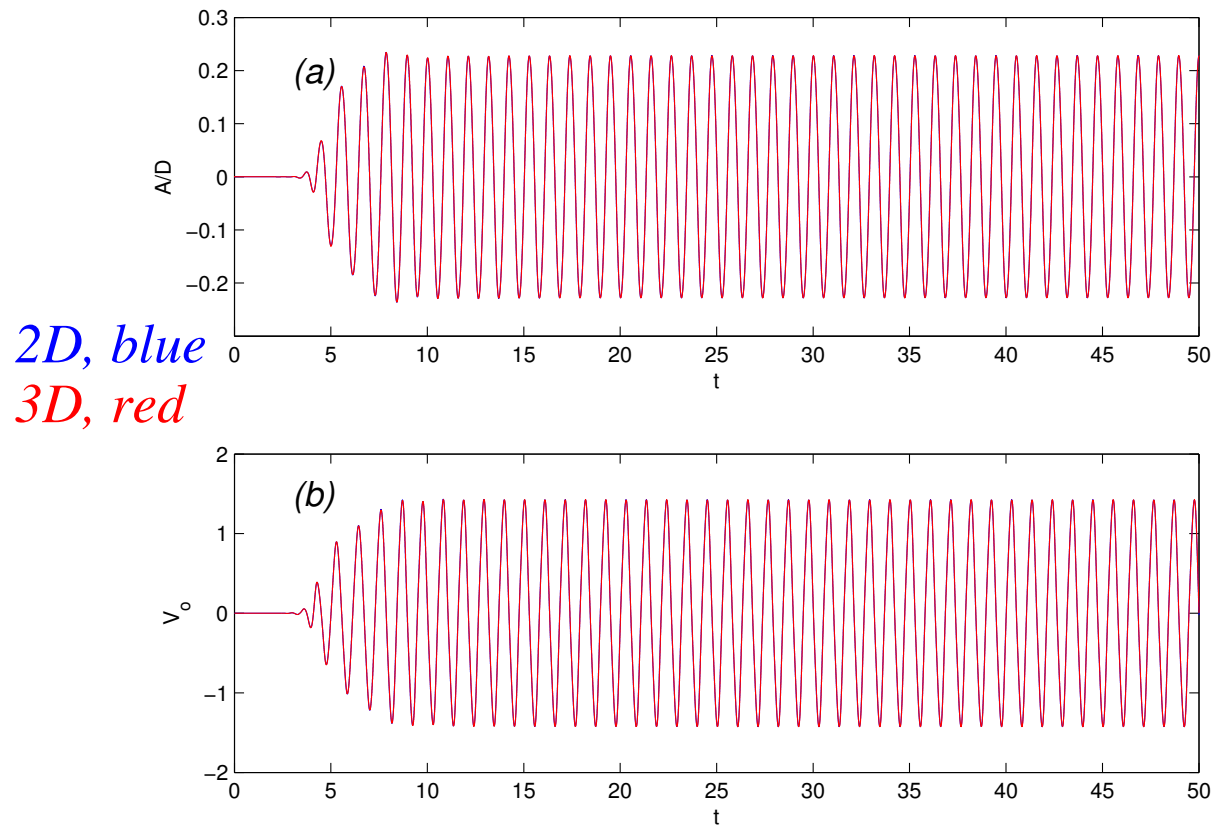
$Re = 200$ results (cont.)

Drag



$Re = 200$ results (cont.)

Cylinder motion



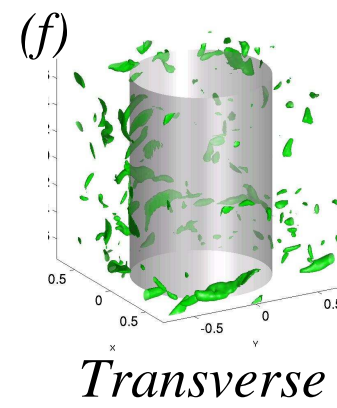
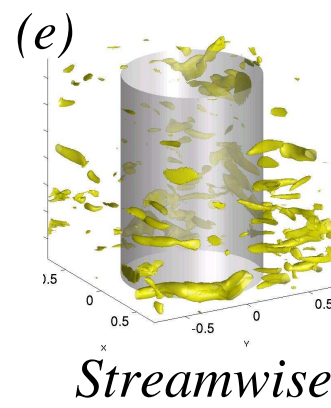
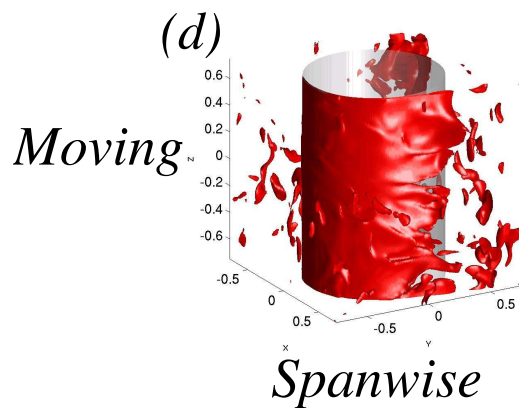
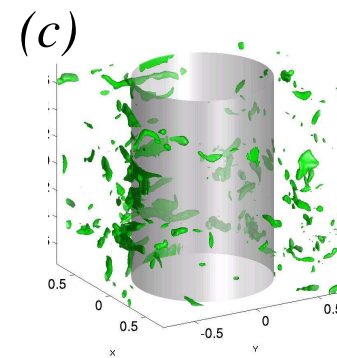
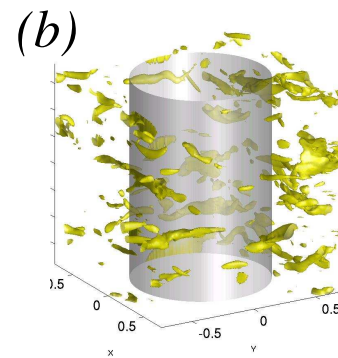
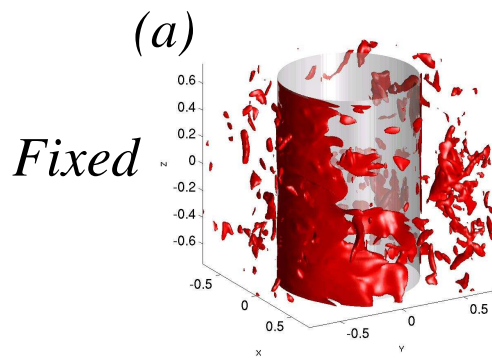
$Re = 200$ results (cont.)

Strouhal frequencies

Case	Peak frequency
2D, fixed	1.32
3D, fixed	1.18
2D, moving	0.95
3D, moving	0.95

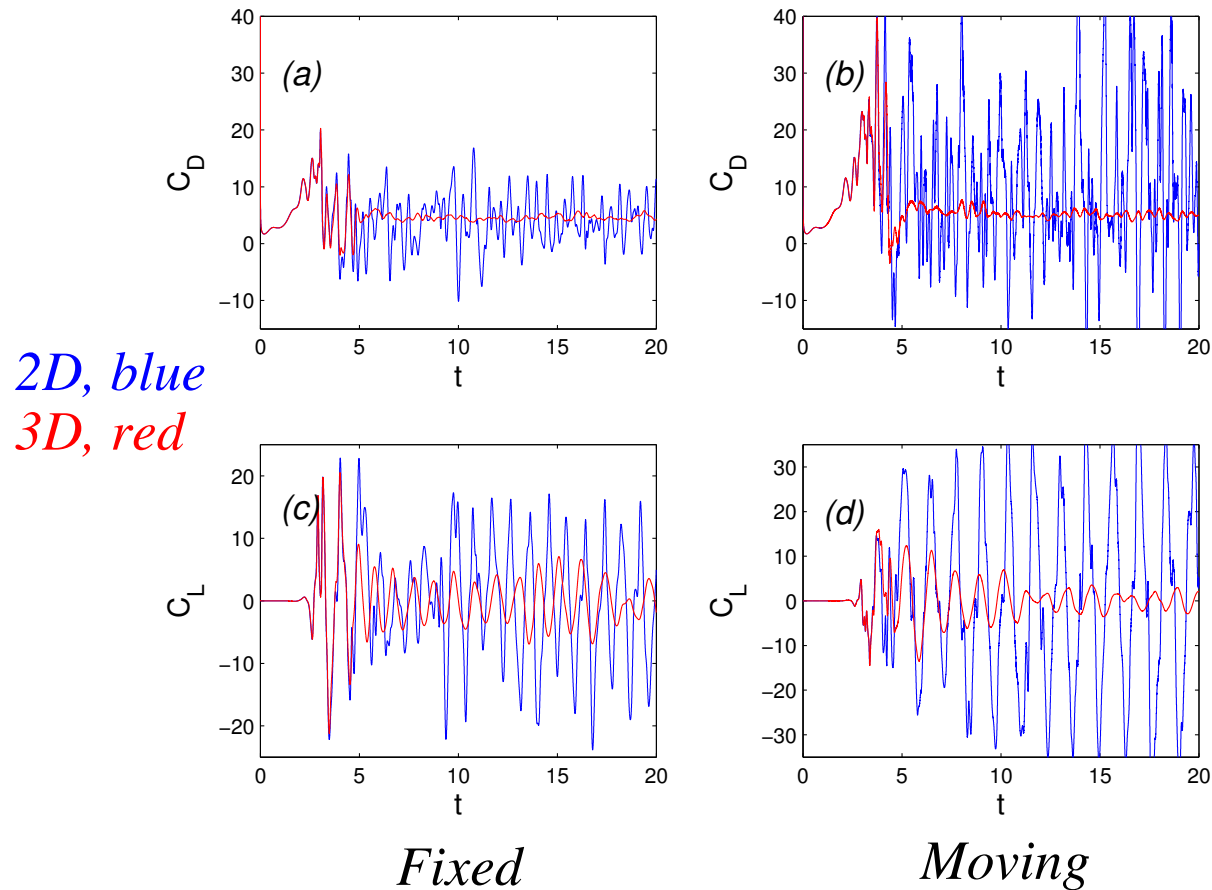
$Re = 1000$ results

Vorticity at $t = 15$



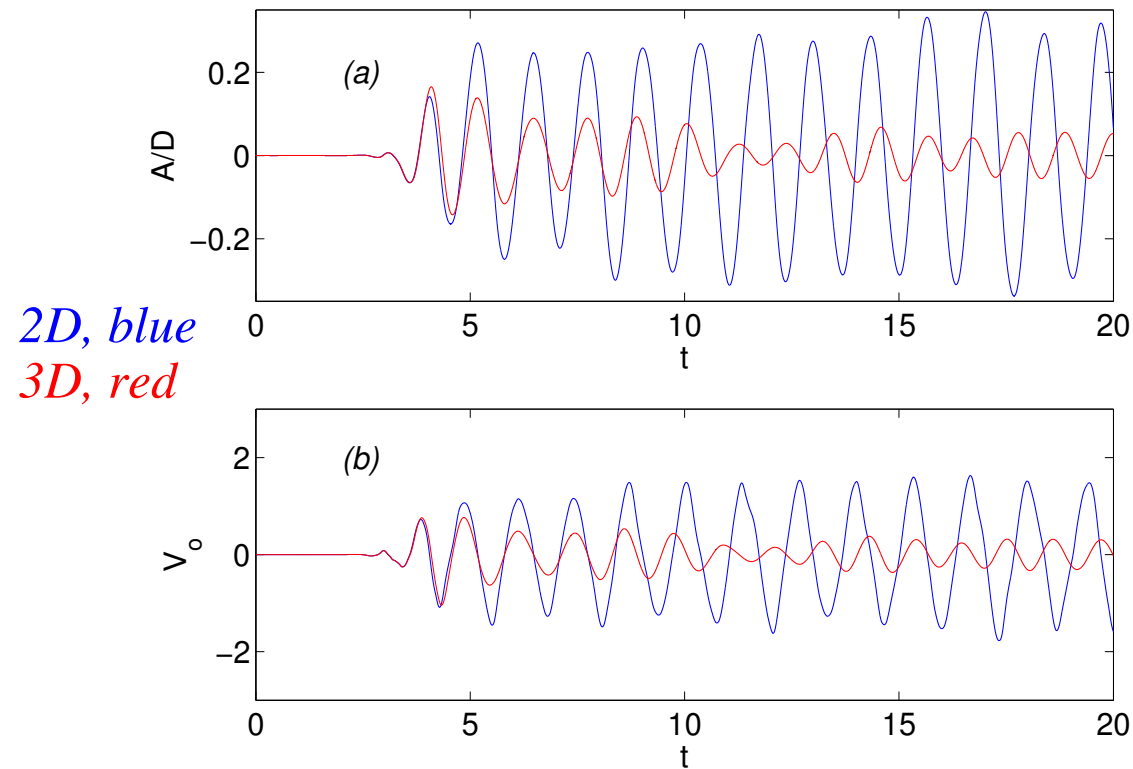
$Re = 1000$ results (cont.)

Lift and drag



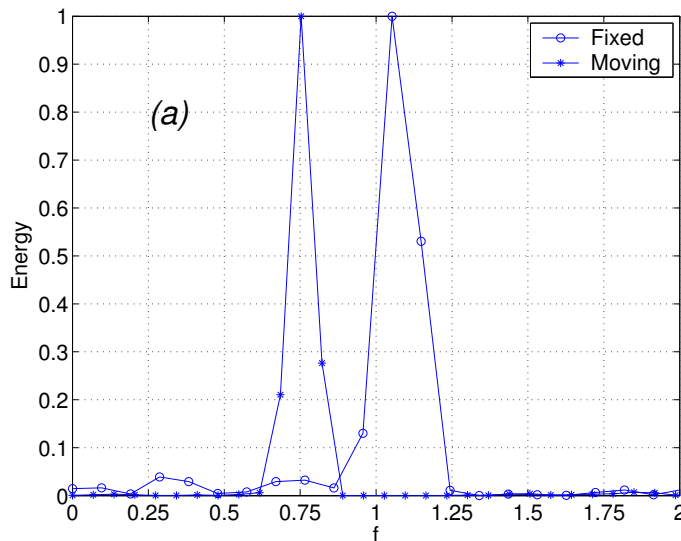
$Re = 1000$ results (cont.)

Cylinder motion

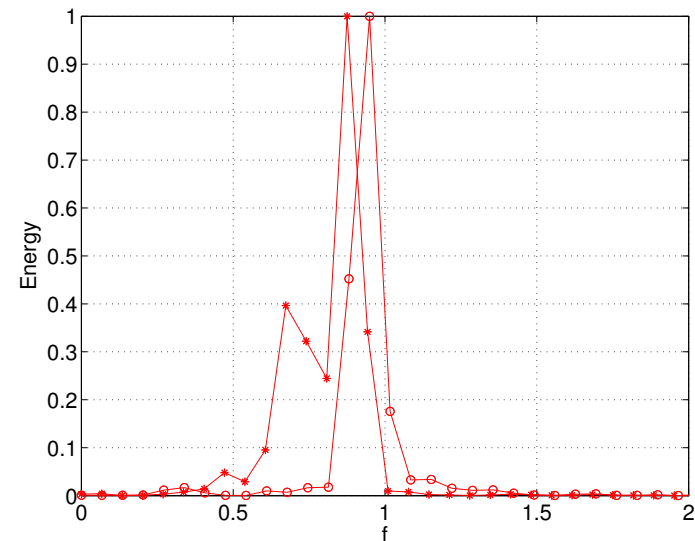


$Re = 1000$ results (cont.)

Lift spectra



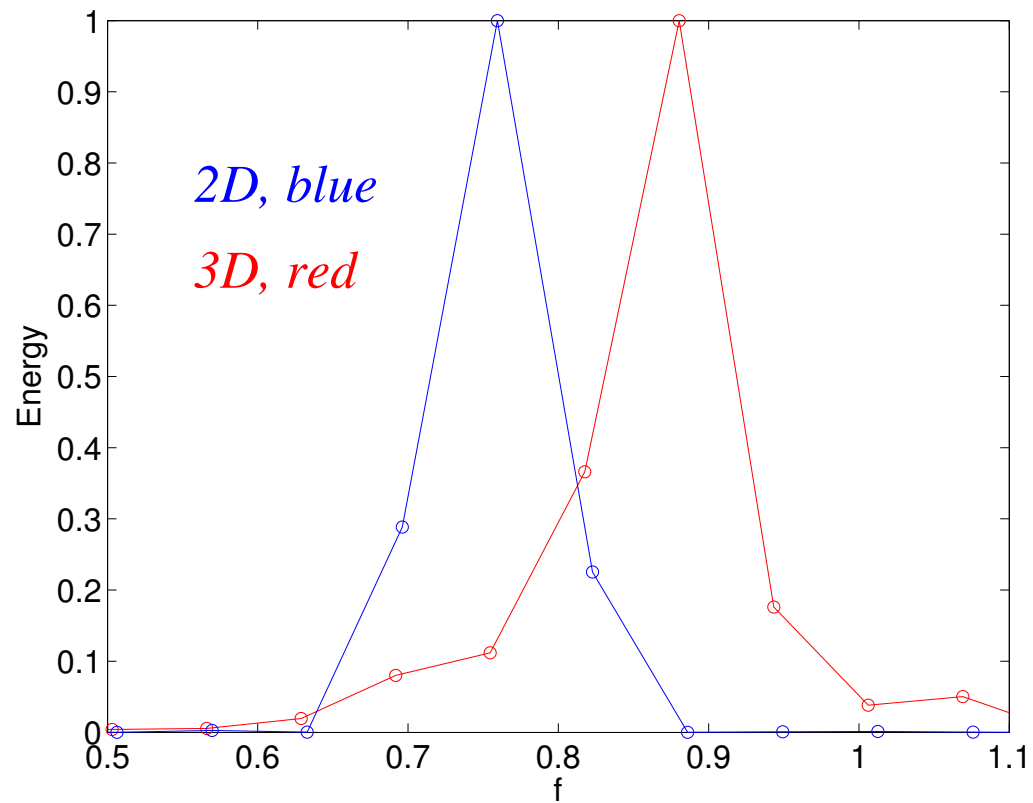
Two-dimensional



Three-dimensional

$Re = 1000$ results (cont.)

Spectra of cylinder oscillation



$Re = 1\,000$ results (cont.)

Strouhal frequencies

Case	Peak frequency
2D, fixed	1.06
3D, fixed	0.95
2D, moving	0.75
3D, moving	0.88, 0.68

Conclusions

Suppression of 3D flow instabilities

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Conclusions

Suppression of 3D flow instabilities

1. At $Re = 200$ cylinder vibration **suppresses** 3D fluid instability ($A/D = 0.23 > 0.125$).
2. **Tight packing** alone does not suppress instability.
3. At $Re = 1\,000$ cylinder vibration is **insufficient** ($A/D \approx 0.05 < 0.125$) to suppress 3D fluid instability.
However, the 2D and 3D Strouhal frequencies and cylinder response **differ only slightly**.

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Conclusions (cont.)

Suppression of 3D flow instabilities (cont.)

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4. **Moving** cylinder has **less effect** at $Re = 1\,000$ than at $Re = 200$.

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Suppression of 3D flow instabilities (cont.)

4. **Moving** cylinder has **less effect** at $Re = 1\,000$ than at $Re = 200$.
5. **Moving** cylinder has **less effect** in 3D than in 2D.

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Conclusions (cont.)

Effect of 3D vorticity compared with 2D flow

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1. Reduces lift amplitude by about **three times**.

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Effect of 3D vorticity compared with 2D flow

1. Reduces lift amplitude by about **three times**.
2. Reduces drag amplitude by about **three times**, and drag is always **positive**. In fact, drag is roughly **constant**.
3. Reduces cylinder amplitude by about **two times**.

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$$Re = 10^4, t = 3.5, P/D = 1.5$$

